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Biochemical Composition and Defensible Bioethanol Production from Seaweed Plentifully Available from Coastal Area of Saurashtra, Gujarat

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ABSTRACT

Acanthophora spicifera (Red algae) and Dictyopteris australis (Brown algae), biomasses were pretreated and subjected to fermentation. Acid pretreatment yielded 35.82±0.12 mg/g and 28.04±0.09 mg/g of reduced sugar respectively. Acid pretreated biomass subjected to enzyme hydrolysis yielded 216 mg/g and 187 mg/g of reduced sugar. Separate hydrolysis and fermentation was carried out for acid hydrolysate using yeast strain isolated from cashew fruit juice (CJY) and toddy juice (TJY) hydrolysate with CJY strain yield 137 mg/g and 107 mg/g respectively of ethanol and TJY yielded 240 mg/g and 190 mg/g respectively for A. spicifera and D. australis of ethanol achieving 26.4 and 20.6 and 47.8 % and 37.4 % theoretical efficiency respectively in SHF process. In SSF process, TJY yielded higher ethanol yield of 470 mg/g and 370 mg/g, achieving 84.2% and 73.7% theoretical efficiency and exhibiting thermo tolerance ability.

Keywords: Acanthophora spicifera (Red algae) and Dictyopteris australis (Brown algae), Bioethanol, SHF, SSF, Thermo tolerance.

Background

Non-renewable fossil fuels triggered serious environmental influence because of that renewable and sustainable energy sources have come into existence (1). Deteriorating fossil fuel has stood intimidation to global economy. An overwhelming increase in the demand for fuel is just because of Population explosion together with increased motorization (2). To improve the environment, bioenergy is an auspicious solution for energy, food and environment problem for the nations which are coal dependent presently and in urgent need of alternative fuels to secure their future (3).

1st Generation biofuel was bioethanol from sugar and starch (sugar cane, maize, corn,

sugar beet). Conversely, huge scale production of this biomass harms the environment by the use of dangerous pesticides, and valuable resources like arable land and enormous quantities of water. World's largest bioethanol renewable resources belonging to 2nd generation biofuel that was bioethanol from lignocellulosic feedstock like industrial and agriculture residue (barley straw, newspaper, and cotton). Biofuel produced using lignocellulosic biomasses originate from agricultural and forest residues (4). However, obstacles in lignocellulosic biomass for conversion to biofuels are cost intensive pretreatment processes due to the presence of lignin molecule. Sustainability of first and second generation biofuels is questioned in connection with food versus fuel argument, carbon accounting

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and land use (5). Therefore, algae are considered as 3rd Generation feedstock for biofuel production. Advantages of algal biomass over first and second generation feedstock's are low land requirement for biomass production and highoil content with high productivity (6).

Aquatic plant (algae) divided into two different groups, micro and macro algae. As the seaweeds do not have lignin at all, the conversion of carbohydrate into ethanol does not require delignification process. As per the characteristics study of seaweeds they are found as the major source for production of bioethanol (7). The production of high concentrations of ethanol from seaweeds requires the conversion of every major carbohydrate into ethanol. In order to produce bioethanol from seaweeds in a cost-effective manner, microorganisms that possess the ability to directly convert polysaccharides (including glucans) into ethanol must be screened or constructed (8).

Microalgae are unicellular found in sea or freshwater ranging from milli to nanometers in size. Macroalgae do not have root, stem, or leaflike macro algae or other aquatic plants, but macro algae or otherwise known as seaweed are found in fresh, or saline water. They are aquatic plants of 50–60 m (9).

Macroalgae are preferred due to its high growth rate, minimum utilization of freshwater and low amount of lignin, allowing efficient processing. Cultivation of macroalgae requires inshore water rather than agricultural land providing a low cost for bioethanol production (10).

According to the specific combination of photosynthetic pigments, they can be classified into three groups: green (Chlorophyta, mainly chlorophyll A and B), brown (Phaeophyceae, mainly chlorophyll A and C, β – carotene and xanthophylls) and red algae (Rhodophyta, mainly chlorophylla, phycoerythrin and phycocyanin) (11).

Red seaweeds are mostly utilized for extraction of carrageenan and agar, whereas alginates are extracted from brown seaweeds. The left over residues rich in cellulose are utilized for biofuel production. Green seaweeds are mostly used for food purpose in Southeast Asian countries (12). Wild strains have ability to convert the seaweed sugars to bioethanol. Highest ethanol yield of 0.31g/g was obtained for TY strain during SSF process (18). Bioethanol has been obtained from all the three types of algae; however study indicates Laminaria japonica, Eucheuma spp., Kappaphycusalvarezii, Undariapinnatifida, and Gracilariaverrucosa as the most promising feedstocks for biorefinery (13).

In India, bioethanol potential from red seaweed species *Kappaphycus alvarezii* (14), *Gracilaria verrucosa* (15) and *Gracilaria corticata* and green seaweed species Ulva fasciata (16), Ulva lactuca (17) have been explored. Bioethanol production process for conversion of algal sugar to ethanol from macro algae involves three major processes such as pretreatment, saccharification and fermentation.

Pretreatment involves acid hydrolysis of the biomass, which alters the structural integrity of the biomass and release sugars. Acid pretreatment increases the accessibility of enzyme for saccharification process; enzymes hydrolyze the cellulose present in algal cell walls to mono saccharides (19). Sugars released after acidic and enzymatic hydrolysis are subjected to fermentation through yeast organism to produce bioethanol (20). Red algae biomass produces the highest amount of bioenergy as compare to other source of biomass (21).

This investigate explores the feasibility of two algae *Acanthophora spicifera* (Red algae) and *Dictyopteris australis* (Brown algae), as suitable feedstock for bioethanol production. Reducing sugar from both acid and enzyme hydrolysis were subjected to fermentation using wild yeast strains.

Methodology Macroalgal sampling

Two algae Acanthophora spicifera (Red algae) and Dictyopteris australis (Brown algae) were collected from the site Lat. and Long. 22.24 N, 68.97 E, Beyt Dwarka, District Devbhumi Dwarka, Gujarat, India, 361350 during low tide period in th e month of March – 2020 (Figure 1, 2 and 3) (https://www.google.co.in/maps/place/Beyt+Dw arka,+Gujarat/@22.1408106,71.1329505,8z/data =!4m5!3m4!1s0x3956bca0fbd18f5f:0x624b9fde4 0601bb9!8m2!3d22.4575896!4d69.1000033).

They were cleaned thoroughly by rinsing in the seawater to remove epiphytes, which were air-dried under shade and oven dried at 60 °C for 5 hrs and pulverized using mortar and pestle, and then sieved to get powder of < 0.1mm. These samples were stored in air tight bags for further analysis.



Figure 1



Figure 2: Acanthophora spicifera (Red algae)



Figure 3: *Dictyopteris australis* (Brown algae)

Systematic position

Acanthophora spicifera (Red algae)

Division: Rhodophyta Class: Rhodophyceae Order: Ceramiales Family: Rhodomeliaceae Genus: Acanthophora Species: Spicifera

Dictyopteris australis (Brown algae)

Division: Phaeophyta Class: Pheophyceae Order: Dictyotales Family: Dictyotaceae Genus: Dictyopteris Species: Australis

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1. Biochemical analysis

Total carbohydrate analysis was performed by phenol-sulphuric acid method (22) followed by the determination of cellulose composition using anthrone reagent method (23). Protein content was estimated by Lowry's method (24). The experiment was performed in triplicates and the mean value was considered for further analyses.

2. Pre-treatment process

Acid hydrolysis: 100mg dried biomass was pretreated with 0.5N H2SO4 at 121°C for 60 min to extract sugars. The hydrolysate was made up to 100ml. After hydrolysis the hydrolysate was neutralize with 2N NaOH to acquire pH 6. The preliminary reducing sugar concentration was calculated using DNS method.

Enzyme hydrolysis: Pretreated biomass was subjected to enzyme hydrolysis using enzyme (S9) extracted from marine bacteria. Enzyme hydrolysis was carried out at 55°C for 36 hr and pH 6.8 (Potassium phosphate buffer). The sugar released was estimated every 6 hr using DNS method.

3. Yeast Isolation and Fermentation

Yeast Isolation: Yeast were isolated from cashew fruit juice (CJY) and toddy juice (TJY) and plated on YEPDA medium of composition 20 g/L peptone, 10 g/L yeast extract, 20 g/L dextrose, 15 g/L agar. Yeast deferment was maintained at 35°C till OD 600 of 0.6 was achieved for further fermentation.

Ethanol fermentation: The hydrolysate obtained from acid pretreatment and enzyme pretreatment were subjected for fermentation using CJY and TJY. Separate hydrolysis and fermentation (SHF) was carried out where hydrolysate (obtained from acid pretreatment and enzyme hydrolysis) were inoculated with 6% v/v yeast seed culture (0.6 OD 600) and sealed with rubber flask to provide anaerobic condition, fermentation was carried out at 28 °C for 24 hr. concurrent Saccharification and Fermentation (SSF) was carried out using 2% (w/v) pretreated biomass and 6% (v/v) enzyme and yeast were added to the medium and fermented using CJY and TJY at 55°C for 24 hr. The ethanol present in the fermented broth was analyze using GC-FID.

RESULTS AND DISCUSSION

3.1. Characterization of Acanthophora spicifera and Dictyopteris australis

During favorable nutrient, salinity, light and temperature condition they grow profusely and occupy intertidal zones. Both the algae were collected from Beyt Dwarka, Gujarat, during the low tide period. Ulva lactuca, green seaweed to enzyme hydrolysis and obtained 112 mg/g of reducing sugar (25). Complementary to dilute acid pretreatment shortcomings are enzyme hydrolysis which do not release inhibitors (26). Higher temperature shortens the exponential phase of the yeast cell resulting in reduced ethanol production (27).

The red macroalgae Acanthophora spicifera has potential bioactive sulfated polysaccharide. It contains galactose (73.5 %), xylose (9.2 %), mannose (1.9 %), arabinose (10.9 %) total sugar (63.3 %) and total sulfate (21.9 %) (28). Spicifera has been identified as very complex as in sulfate. In the Brown algae - Dictyopteris australis. some species show a distinct photochemistry, with specific secondary metabolites, including C11-hydrocarbons, sulfur compounds and quinone derivatives, not usually found in marine seaweeds and described for the first time in the literature. Protein content, total sugar and fat contents ranged between 14.4 % and 23.8 %, 32.4 % and 49.3 % and 0.6-3.6 % (29, 30).

3.2. Pretreatment

3.2.1. Dilute acid hydrolysis

Dilute acid pretreatment is most widely used process for extraction of reducing sugars from biomass. However drawback of this is degradation of sugars in to inhibitors such as hydroxyl methyl furfural (HMF). Biomass treated using dilute acid yielded 35.82±0.12 mg/g and 28.04±0.09 mg/g of reducing sugar respectively. Pretreatment improves porosity of the biomass and decreases the crystallinity of the biopolymer cellulose. Complementary to dilute acid pretreatment shortcomings are enzyme hydrolysis which do not release inhibitors. Pretreatment of biomass is done to expose the cell constituents and cell wall materials for enzyme action. Bhatt et al.

3.2.2. Enzyme hydrolysis

Enzyme hydrolysis was performed for acid pretreated *Acanthophora spicifera* and *Dictyopteris australis*, yielded 216 mg/g (Figure 4) and 187 mg/g (Figure 5), isolated cellulase enzyme from Cladosporium sphaerospermum and subjected Ulva lactuca, green seaweed to enzyme hydrolysis and obtained 112 mg/g of reducing sugar. Subjected hydro thermally pretreated E. in testinalis to enzyme hydrolysis using commercial



3.3. Fermentation 3.3.1. Separate hydrolysis and Fermentation (SHF)

Fermentation was carried out for *Acanthophora spicifera* and *Dictyopteris australis* by SHF method for 24h. Hydrolysate obtained from acid pretreatment was subjected to fermentation. Ethanol yield of 137 mg/g and 107 mg/g were obtained from 3.58 g and 2.80 g reducing sugar and theoretical efficiency of 26.40 % and 20.65 % respectively were achieved for hydrolysate with CJY strain (table 1). Hydrolysate with TJY strain yielded ethanol of 240 mg/g and 190 mg/g achieved from 3.32 g and 2.60 g reducing sugar and theoretical yield of 47.81 % and 37.44 % efficiency were achieved. TJY strain yielded higher efficiency than CJY strain indicating its potential in producing ethanol from seaweed.

3.3.2. Simultaneous Saccharification and Fermentation (SSF)

Higher ethanol yield were observed in SSF for ASTJY 470 mg/g and for DATJY 370 mg/g whereas

enzymes Viscozyme L and Cellic CTec2 and obtained 20.1 g/L of reducing sugar. Reduced sugar were seen to increase linearly with incubation period from 12 to 24 hr ranging from 75 mg/g to 213 mg/g, and decreased beyond 24 h to 116 mg/g for *Acanthophora spicifera* and for *Dictyopteris australis* RS increase linearly with incubation period from 12 to 24 hr ranging from 62 mg/g to 185 mg/g, and decreased beyond 24 h to 96 mg/g. (17).



for ASCJY 210 mg/g and for DACJY 160 mg/g of ethanol yield were recorded (Table 1). SSF operated at higher temperature of 55°C as enzyme gets activated at this temperature. TJY strain exhibited tolerance to higher temperature and yielded higher ethanol.

3.4. Other value added properties of selected plants

Acanthophora spicifera, have anticoagulant and antiplatelet. A. *spicifera* and commercial products inhibited aggregation of platelets and coagulation of plasma, and thus they have anti hemostatic properties (30).

Research on the Dictyopteris species, hundreds of metabolites have been isolated, includeing many unique molecules, such as uncommon sulfur compounds and meroditerpenes, which were reported for the first time. The biological activities reported to some Dictyopteris species suggest them to have a high medicinal potential (31).

| Process | Substrate | Initial | Final | Fermented | Ethanol | Ethanol | Theoretical |
|--|---------------|---------|-------|-----------|---------|---------|-------------|
| | | Sugar | Sugar | Sugar | (g/L) | Yield | Yield (g/L) |
| | | (g/L) | (g/L) | (g/L) | | (g/L) | |
| Estimation of ethanol Acanthophora spicifera | | | | | | | |
| SHF | EI CJY | 3.58 | 0.88 | 2.69 | 0.237 | 0.137 | 26.40 |
| | EI TYJ | 3.32 | 1.19 | 2.12 | 0.339 | 0.24 | 47.81 |
| SSF | EI CJY | 14.92 | 2.61 | 12.30 | 1.73 | 0.21 | 42.35 |
| | EI TYJ | 15.18 | 4.30 | 10.87 | 3.41 | 0.47 | 84.26 |
| Estimation of ethanol Dictyopteris australis | | | | | | | |
| SHF | EI CJY | 2.80 | 0.69 | 2.10 | 0.185 | 0.107 | 20.65 |
| | EI TYJ | 2.60 | 0.93 | 1.66 | 0.265 | 0.19 | 37.44 |
| SSF | EICJY | 11.67 | 2.04 | 9.62 | 1.35 | 0.16 | 33.12 |
| | EI TYJ | 11.87 | 3.36 | 8.50 | 2.67 | 0.37 | 73.31 |

Table 1: Estimation of ethanol

Conclusion

Macroalgae is an attractive biomass for bioethanol production as they are rich in carbohydrates which can be readily converted to bioethanol using appropriate yeast microorganisms. Wild strains have ability to convert the seaweed sugars to bioethanol. Highest ethanol yield of 470 mg/g and 370 mg/g were obtained for TJY strain during SSF process indicating thermo tolerance nature of TJY strain.

Acanthophora spicifera and Dictyopteris australis are widely distributed along intertidal zones of bays and coastal ecosystem. Growth rate of Acanthophora spicifera and Dictyopteris australis reaches up to 3.60 % and 7.80 % per day.

Similarly, in Beyt Dwarka, District Devbhumi Dwarka, Gujarat, *Acanthophora spicifera* and *Dictyopteris australis* are recorded in large quantities along the intertidal zone during monsoon and post monsoon. Availability of such large biomass quantity can be tapped for bioethanol production

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